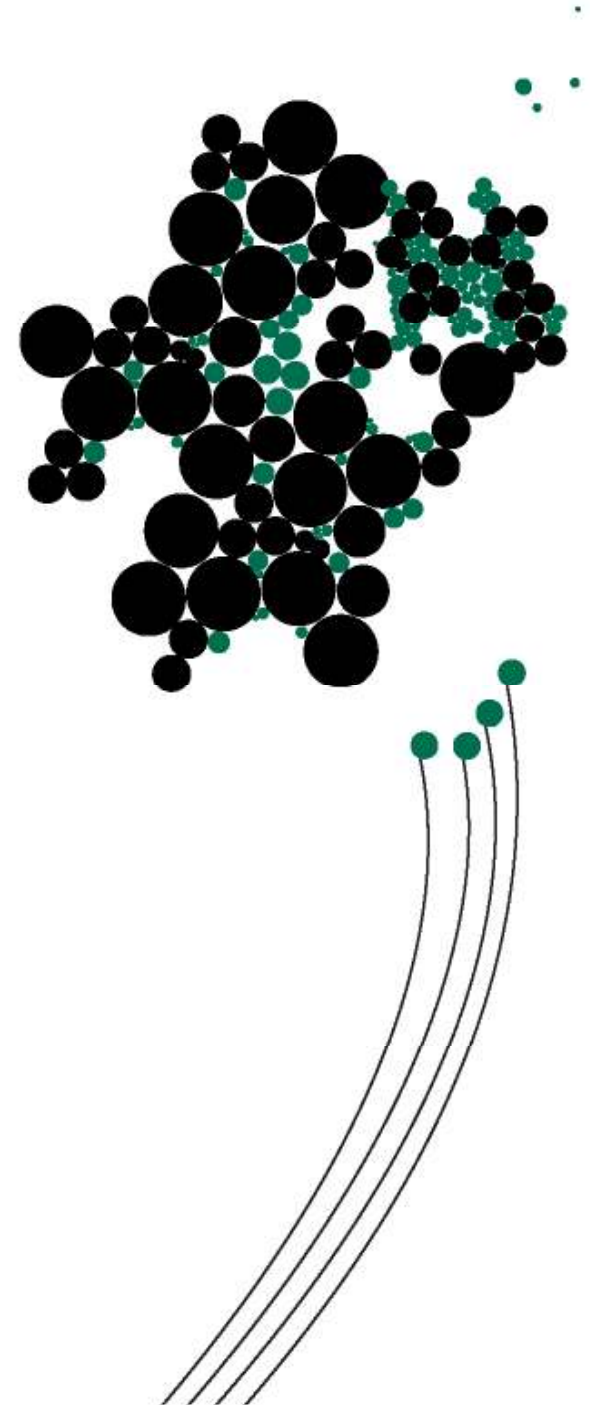


# IMPACT

*Biomass Research at TCCB*

**UNIVERSITY OF TWENTE.**

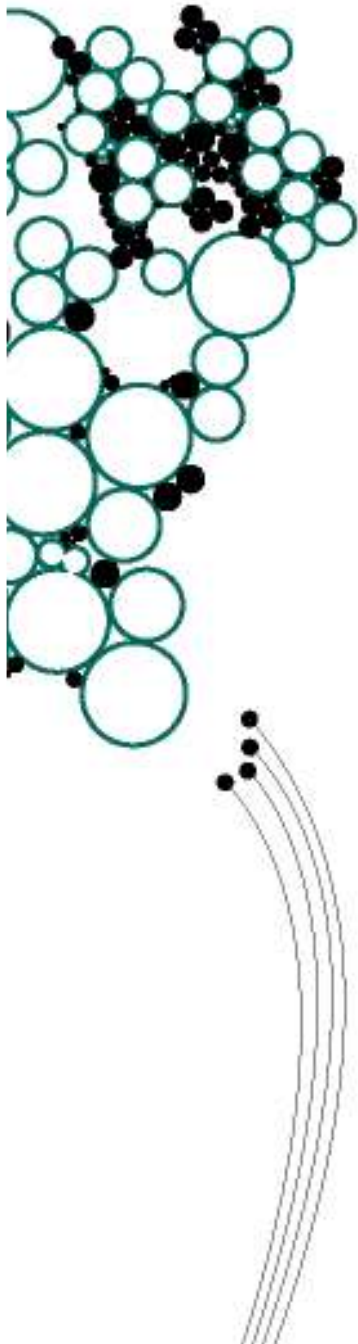


# Biomass Research at the University of Twente

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- Since 1972 biomass research
- Now: 40 fte researcher (PHD, post-doc)
- Research disciplines:
  - Process Technology
  - Catalysis
  - Separations
  - Chemistry/Materials
  - Socioeconomics
- Funding: university board, subsidy agents (local, national, international), companies





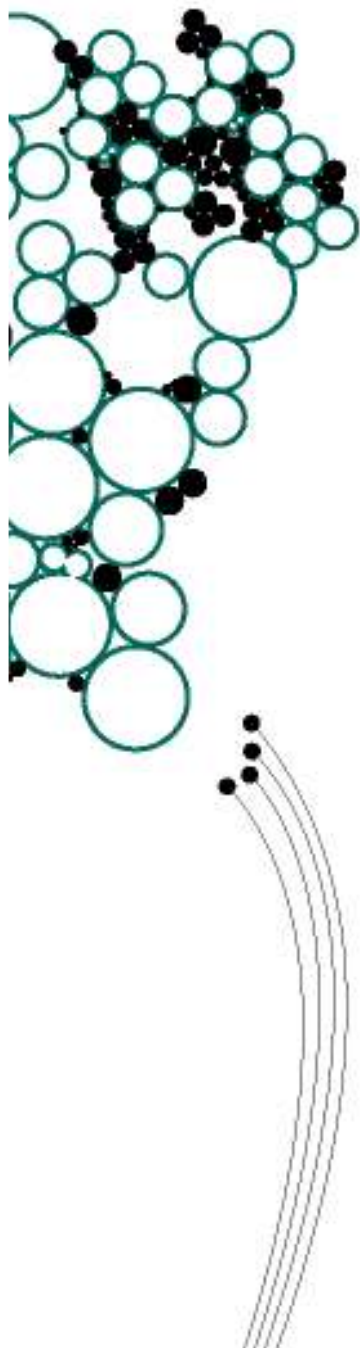
## Biomass Province Overijssel

- Biomass available
- Companies
  - Biomass collection
  - Technology owners
  - Biomass users



- Support by the Provincial Government
  - Initiating and financing a centre for Research and Innovation













# People

UNIVERSITY OF TWENTE.





## SCIENTIFIC STAFF

- Prof.dr. S.R.A. Kersten 
- Prof.dr.ir. H. van der Berg 
- Dr.ir. D.W.F. Brillman 
- Dr.ir. A.G.J. van der Ham 
- Dr.ir. J.A. Hogendoorn 
- Dr.ir. G. van Rossum 
- Prof.dr.ir. W.P.M. van Swaaij 




## SECRETARY

- Y.C.H. Bruggert-ter Huurne 





## TECHNICAL / ANALYTICAL STAFF

- J.F.H. Agterhorst 
- K. van Bree 
- Ing. E. Fränzel 
- B. Knaken 

## POST-DOC / VISITING

- Dr.ir. A.M.J. Kootstra 
- Dr. J.A. Medrano Catalan 
- D.I. Habeych Narvaez PdEng. 

## PHD

- Ir. N. Aldenkamp 
- P. Balegedde MSc. 
- M. Castellvi Barnes 
- A. Chakinala MSc. 
- L. Garcia Alba MSc. 
- Ir. E. Hoekstra 
- M.E. Majchrowicz MSc. 
- Ir. P. Nanou 
- MSc. 
- Ir. R.J.M. Westerhof 
- R. Veneman 

## MASTER / BACHELOR / EXCHANGE

- P. Bode 
- E. van den Dries 
- H. Gutierrez Murillo 
- P. Meijerink 
- S. Oudenhoven 
- F.N.H. Schrama 
- X. Shushil 
- A.J. de Weerd 
- M.P. Vos 
- R. Azhar 
- T.A. Berk 
- J.F.D. Boegborn 
- M.J. Bos 
- C. van Foeken 
- J. de Graaf 
- M. Kropman 
- K.J. Lo 
- R.R. Scholte op Reimer 
- M.M. de Visser 

# Research

## Biomass



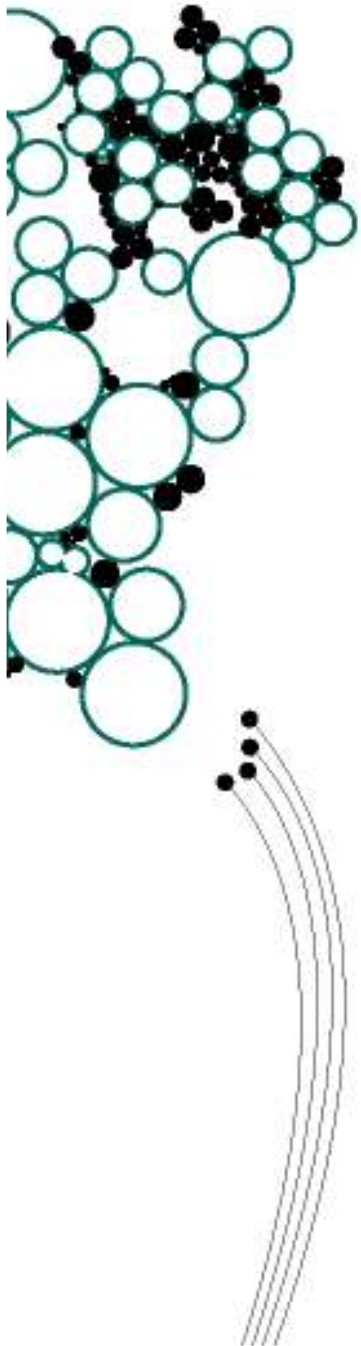
**Thermo-chemical conversions**  
**Catalytic Conversions**  
*Biotechnological conversions*  
**Separations**  
**Non-technical aspects**

CO<sub>2</sub> / C-source  
Photons  
Electrons

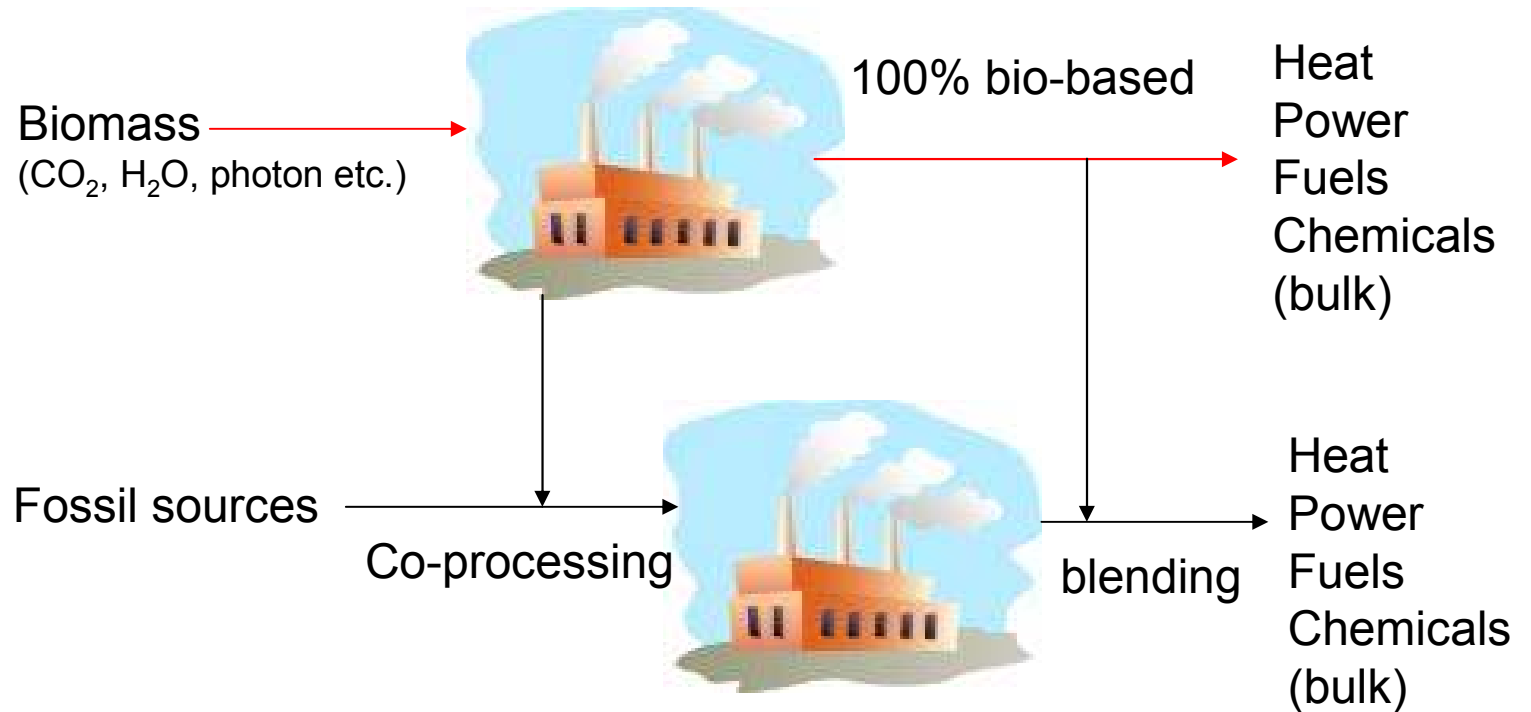
Heat  
Power  
Fuels  
Chemicals



Fossil feeds



# 100% biobased or integrating with fossil industry







# Feedstocks

## 1<sup>st</sup> generation



**Sugar Cane**  
(Current Biofuels)

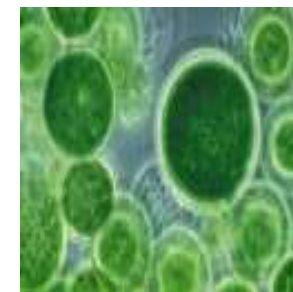


**Forestry residues**

## 2<sup>nd</sup> generation



**Agricultural residues**



**Energy Crops**

## 3<sup>rd</sup> generation

Photons  
Electrons  
CO<sub>2</sub>  
H<sub>2</sub>O  
C-source



(intermediate)  
products

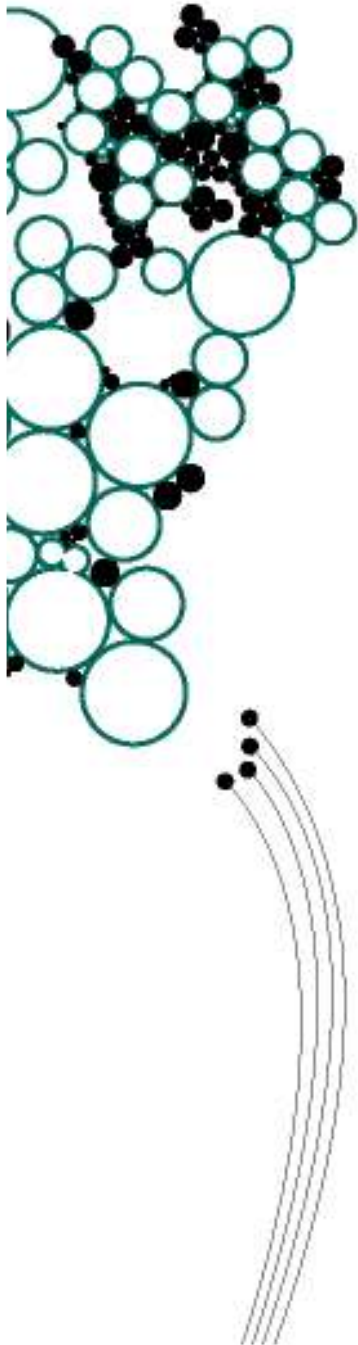


## Research Topics

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- Primary Thermo-chemical / catalytic conversions
  - Liquefaction
  - Gasification
  - Torrefaction
- Upgrading (thermal/chemical/catalytic) of bio-gases and liquids to fuels and chemicals
- Algae production and refinery
- Separations (for fuels and chemicals production)
- E-Fuels
- Artificial photosynthesis (engineering part)
  
- P-recovery/recycling
- Affinity separations
- Desalination





## Scales of Production and Processing

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### Current Conversion Scales

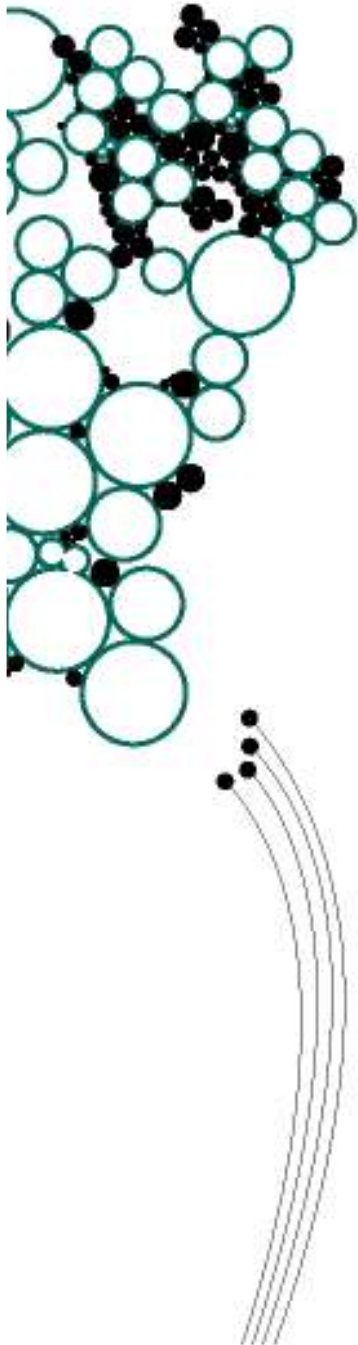
- Large Scale Central
  - Power plants: 0.5 – 2 GW
  - Refinery : 2 - 40 GW
    - 10% chemicals
    - 20% energy
    - 70% fuels
  - Chemical plants 0.1 – 2 GW

### Biomass Production / Availability

- Farm (100 ha): 1.5 MW
- Sugar plantation: 0.5 – 2 GW
- Wood farming: 10MW – 1 GW
- Paper mill: 0.05 – 1 GW

(Small) Refineries and chemical plants fit  $\longrightarrow$  Co-processing  
on the largest farming complexes and paper mills

Small scale availability requires  
pretreatment and very efficient logistics



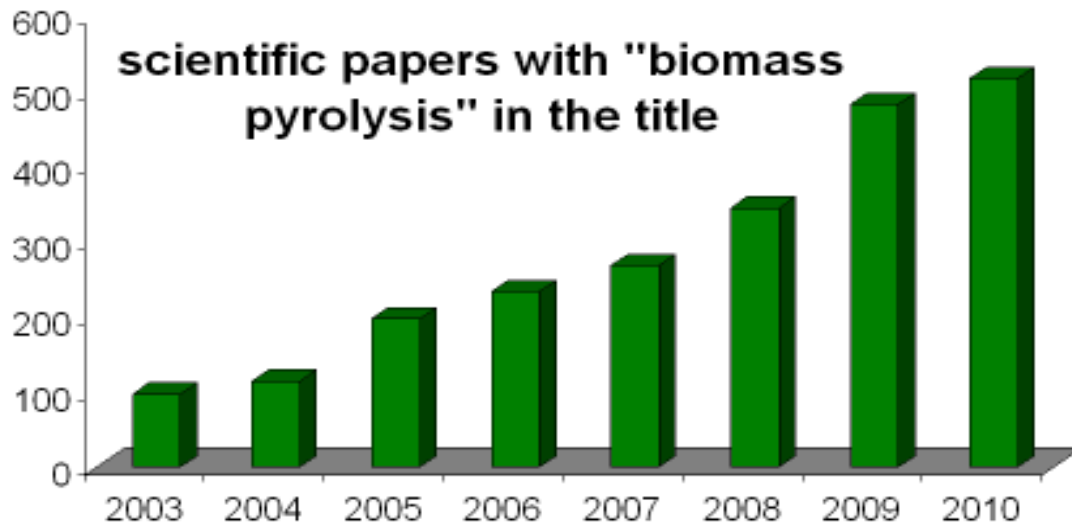
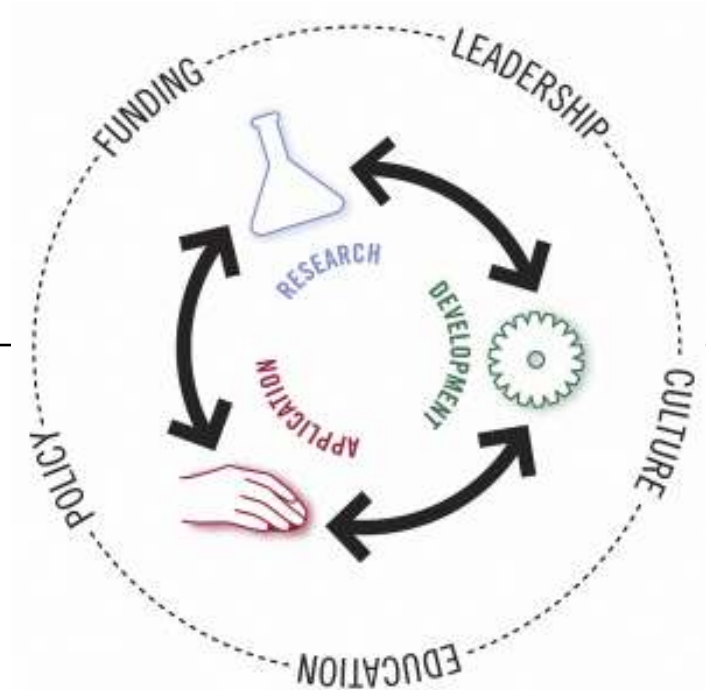
## In 2050 Biomass is used for:

- Food
- Feed
- Dedicated liquid fuels
  - Long distance heavy transport (short distance → electric)
  - Aviation (jet fuel)
- Chemicals & Materials
  - Acids
  - Ethylene / propylene
  - aromatics
  - Plastics
  - Specialties....

Energy Storage Systems		
	MJ/L	MJ/kg
<b>Gasoline</b>	<b>32</b>	<b>43</b>
<b>Methanol</b>	<b>17</b>	<b>21</b>
<b>Ethanol</b>	<b>22</b>	<b>28</b>
<b>Liquid hydrogen</b>	<b>8.4</b>	<b>120</b>
<b>Hydrogen 350 bar</b>	<b>2.8</b>	<b>120</b>
<b>Hydrogen hydride</b>	<b>13</b>	<b>6</b>
<b>Lead battery</b>	<b>0.24</b>	<b>0.12</b>
<b>Li-ion battery</b>	<b>1.2 - 2</b>	<b>0.84</b>

## Innovation Gap

Implementation needed  
to improve technology

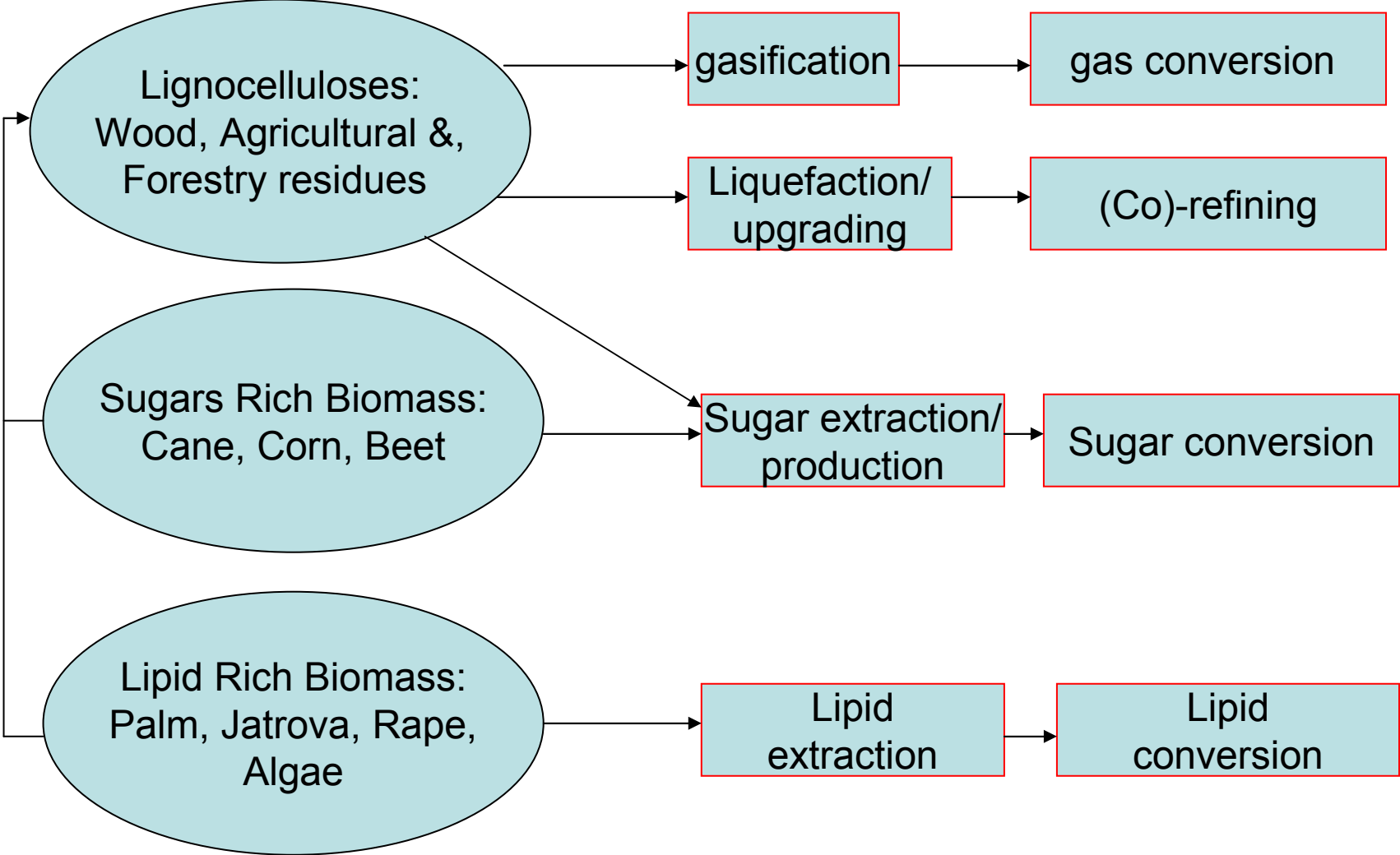


1

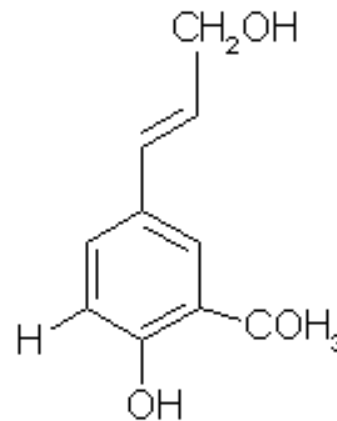
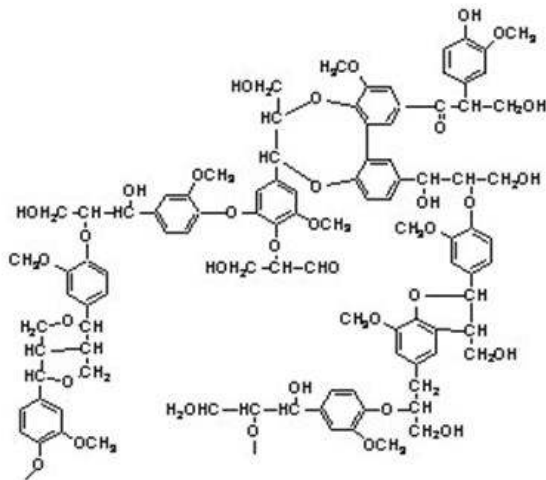
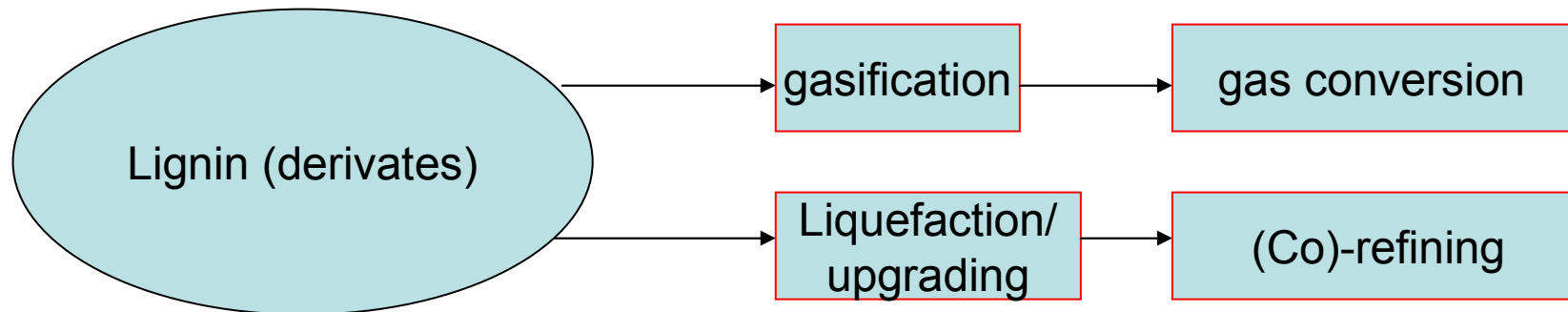
Number of commercial  
pyrolysis plants 2011

In a perfect world, strong technological concepts would always evolve into commercial reality. But that ideal is relatively rare#.

# Processing Routes to Fuels & Chemicals

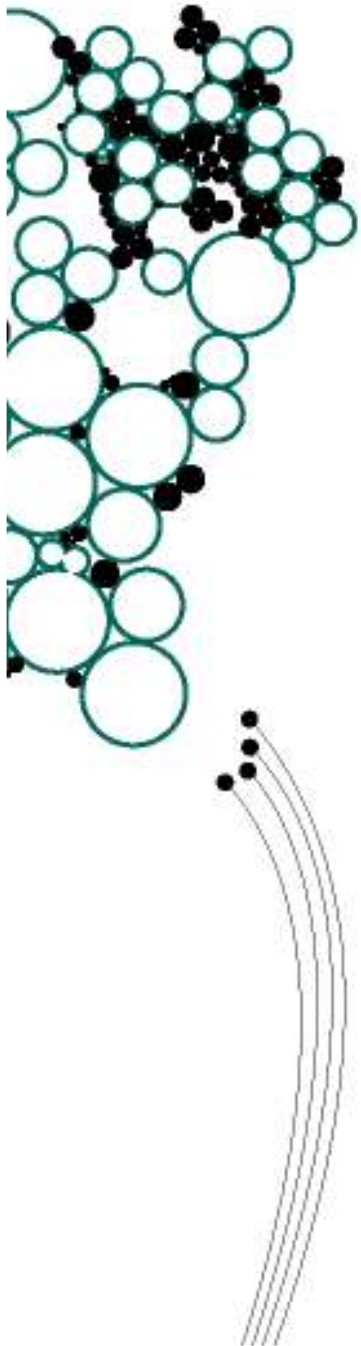


## Processing Routes to Fuels & Chemicals (cont.)

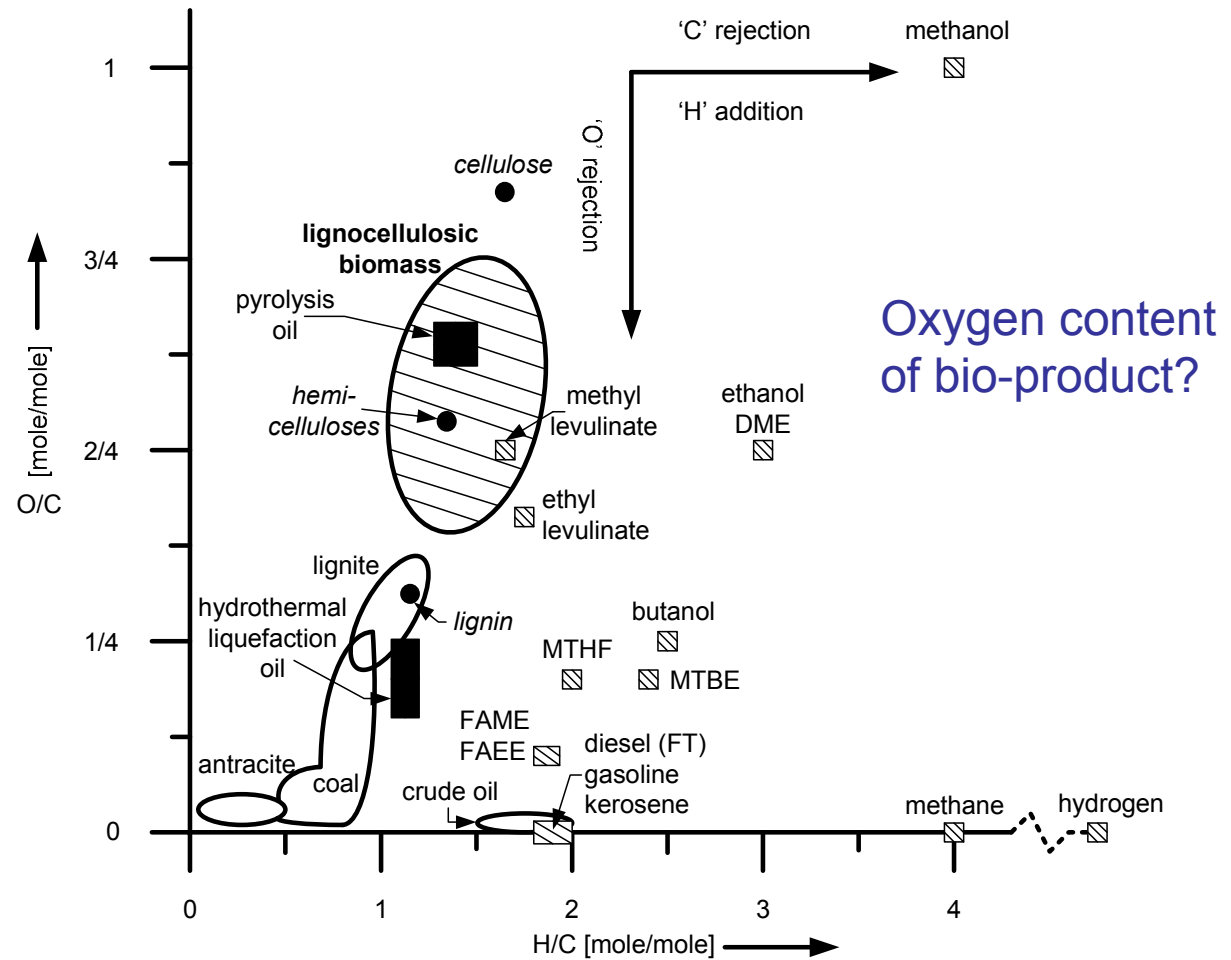


Lignin subunit: Coniferyl Alcohol

**Chemicals**  
**- Aromatics**  
**- Propylene**

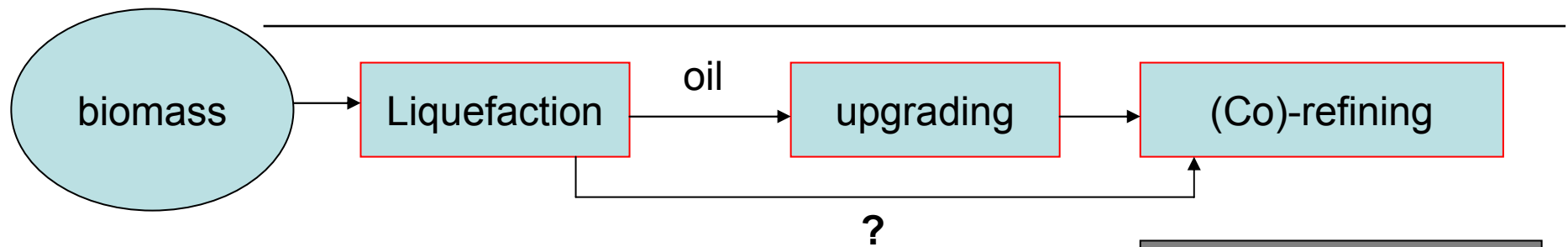


# What type of Fuels?





## Oil from Residues



- Liquefaction (making biomass liquid)
  - Mimicking nature
  - Increased volumetric energy density (5x)
    - Transport easier and cheaper
  - Liquids easier to process
  - Enables refinery
  - Minerals (fertilizer) remain in a by-product (return to soil)
  - Enables decentralized biomass pretreatment nearby biomass production locations
  - Central refinery

Oil is liquid biomass:

50 wt% C

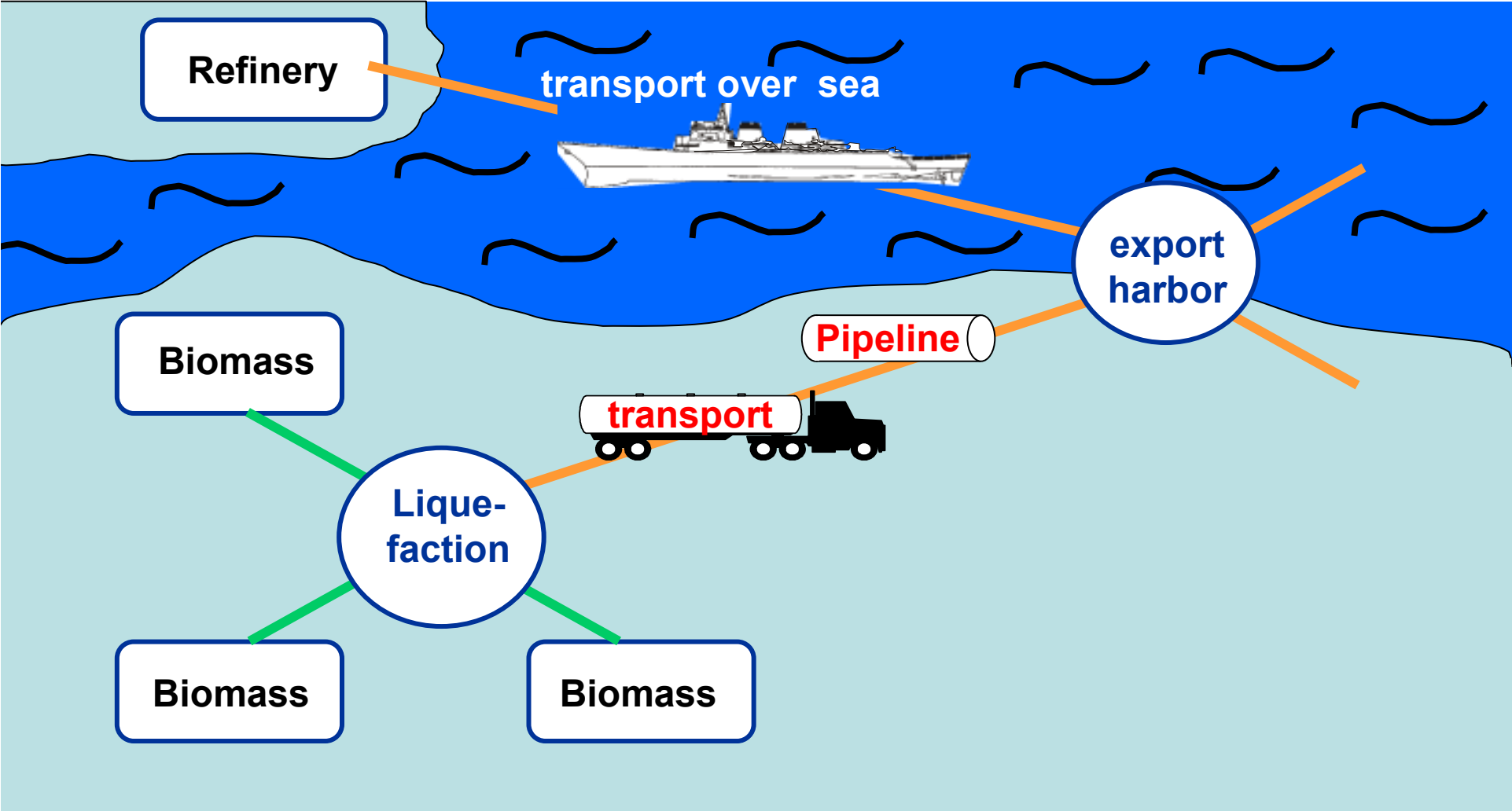
6 wt% H

44 wt% O

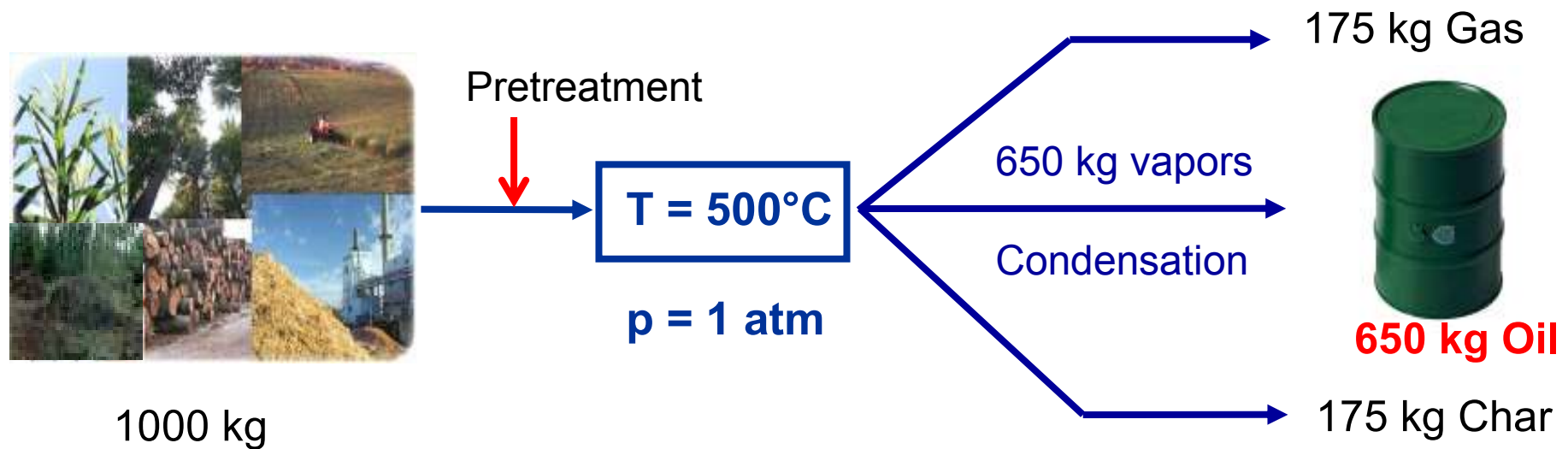
1 MJ



# Decentralized Pretreatment & Central Refining

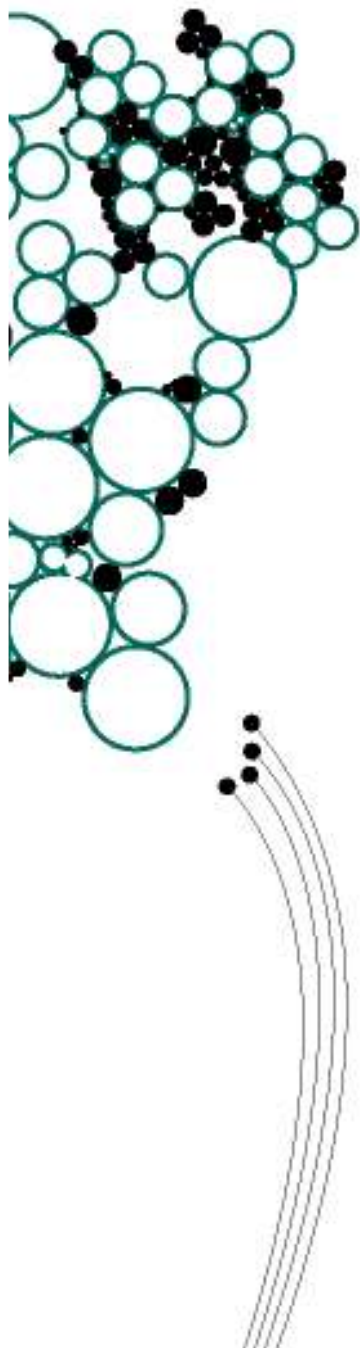


# Pyrolysis



- Research at UT since 1985
  - Process development
  - Oil quality
  - Oil applications
- Commercialization by companies (BTG)
  - 5 ton/hr Plant in 2012 in Hengelo (OV)

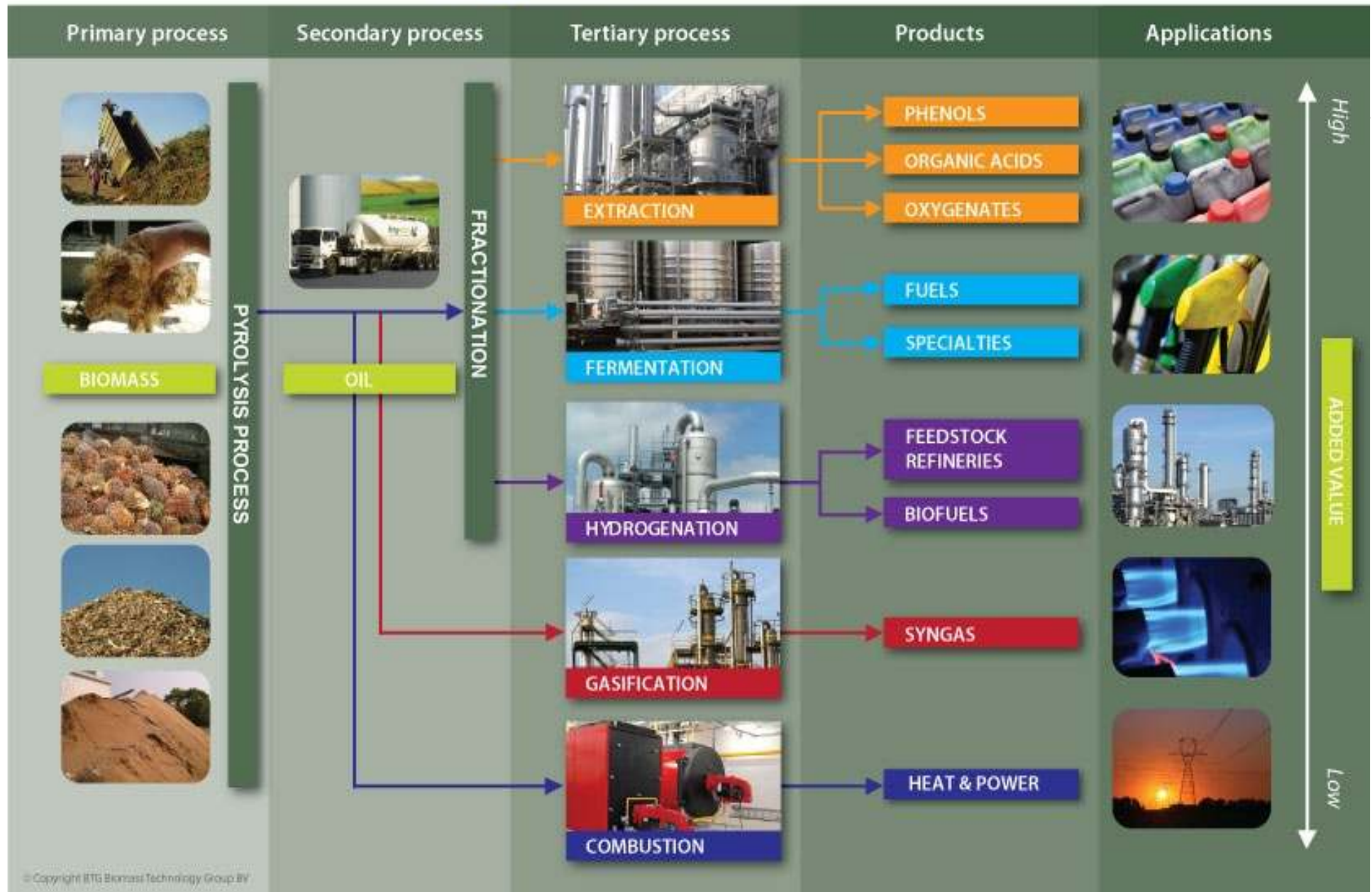




## Pyrolysis Oil

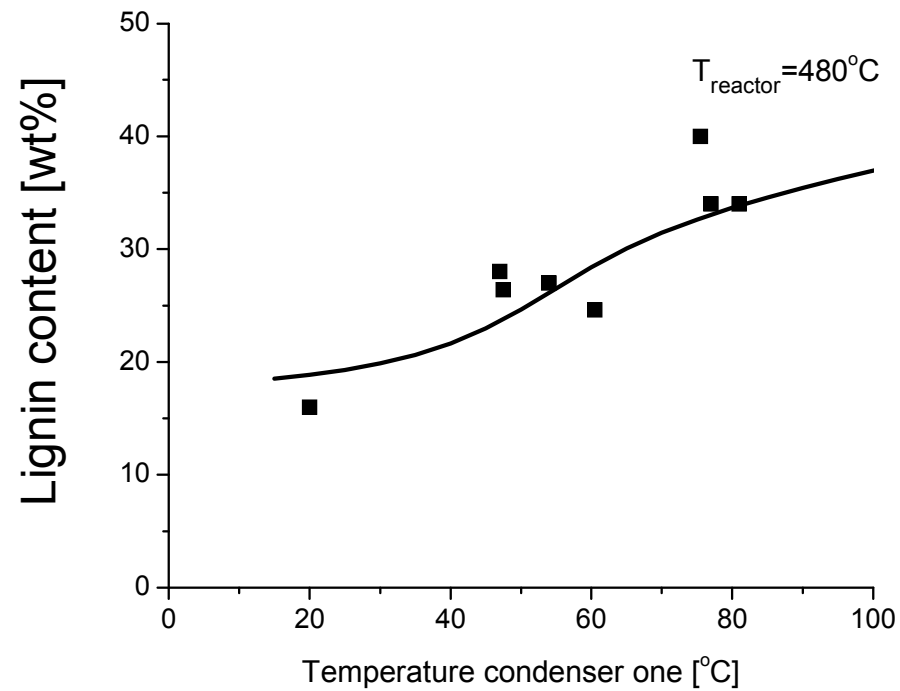
**Physical Characteristics and Elemental Composition of Pyrolysis Oil, Hydrothermal Liquefaction Oil, and Fossil Heavy Fuel Oil**

Characteristic	Pyrolysis Oil	Hydrothermal Liquefaction Oil	Heavy Fuel Oil
Water content (w%)	15-35	3-6	0.1
C (w%, dry)	50-64	65-82	85
H (w%, dry)	5.2-7	6-9	11.1
O (w%, dry)	35-40	6-20	1.0
N (w%, dry)	0.05-0.4	nd	0.3
S (w%, dry)	0.05-0.3	nd	2.3
Heating value (MJ/kg) (LHV)	16.5-19	25-35	40
Viscosity (cp at ~50°C)	40-150	~10 <sup>4</sup>	180
pH	2.4	--	--
Total acidity number (TAN)	70-150	nd	--
Specific gravity	1.15-1.25	1.05-1.15	0.90
MW (g/mol)	600-700	500-1000	180-400



## Lignin is present in pyrolysis oil (emulsion)

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# Pyrolysis: Process Development Units at UT

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PyRos pilot plant – 30 kg/hr

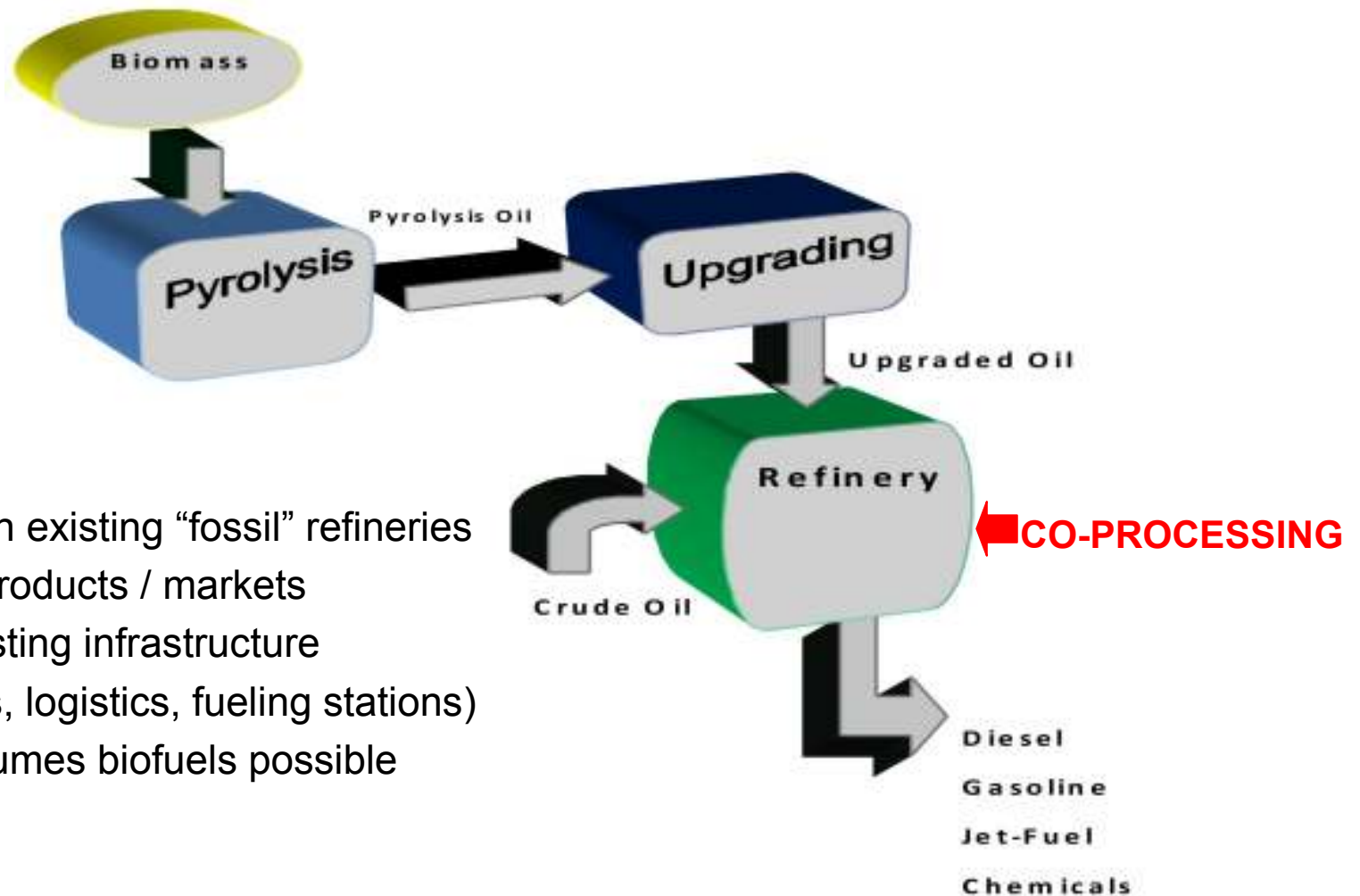


Fluid bed – 1 kg /hr



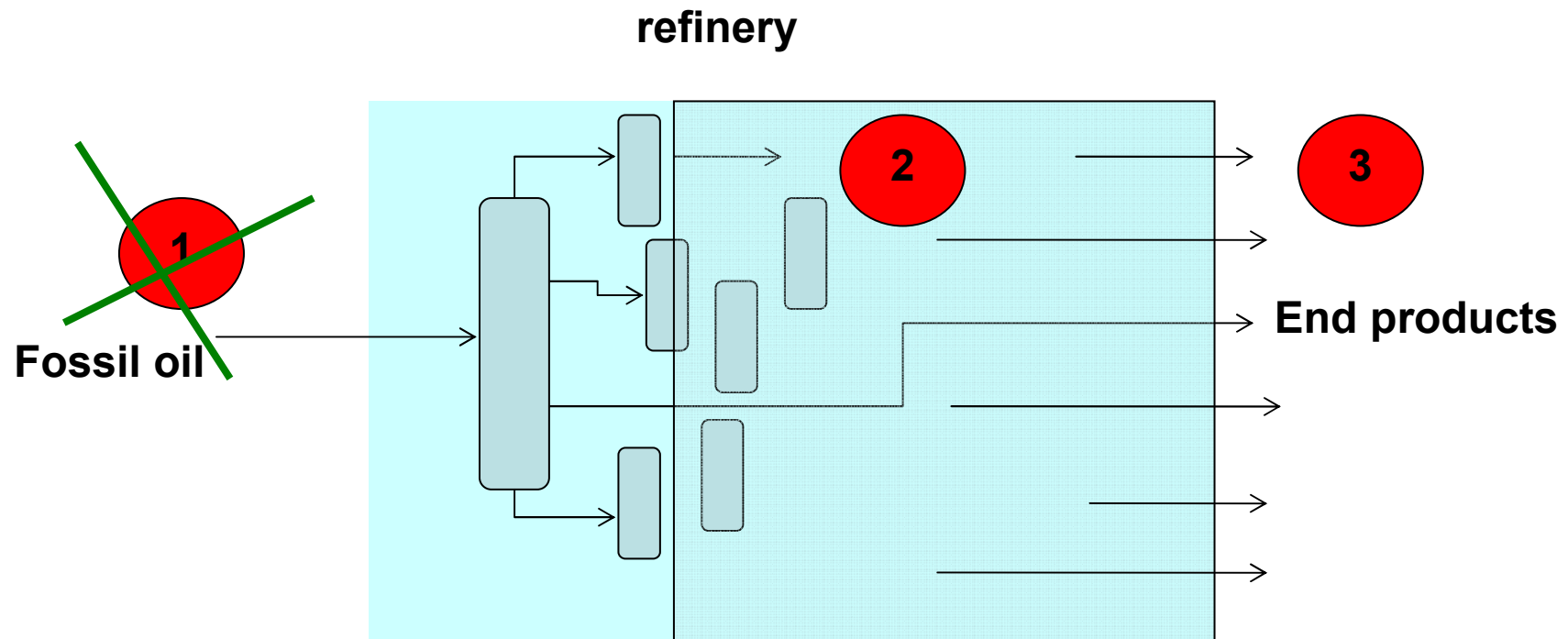
## Co-Processing Pyrolysis Oil in Crude Oil Refineries

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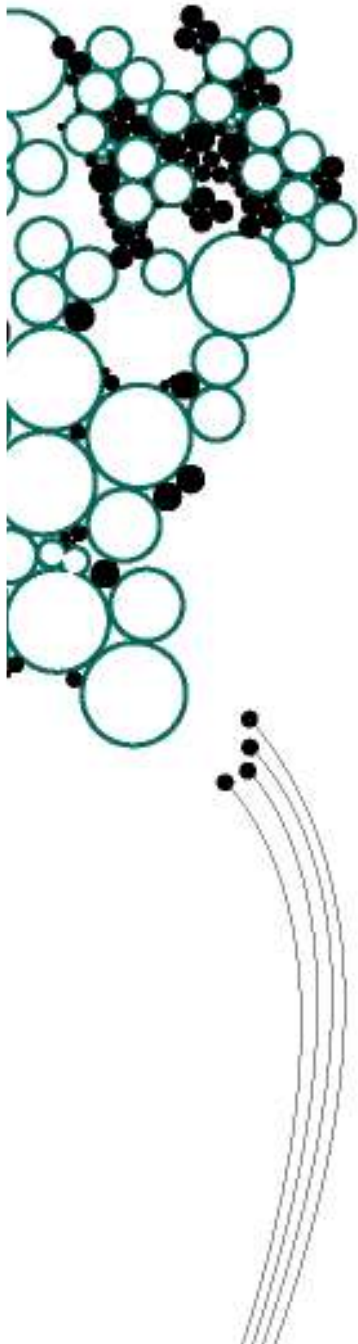


- Partnering with existing “fossil” refineries
  - Existing products / markets
  - Using existing infrastructure (refineries, logistics, fueling stations)
  - Large volumes biofuels possible

# Co-processing options



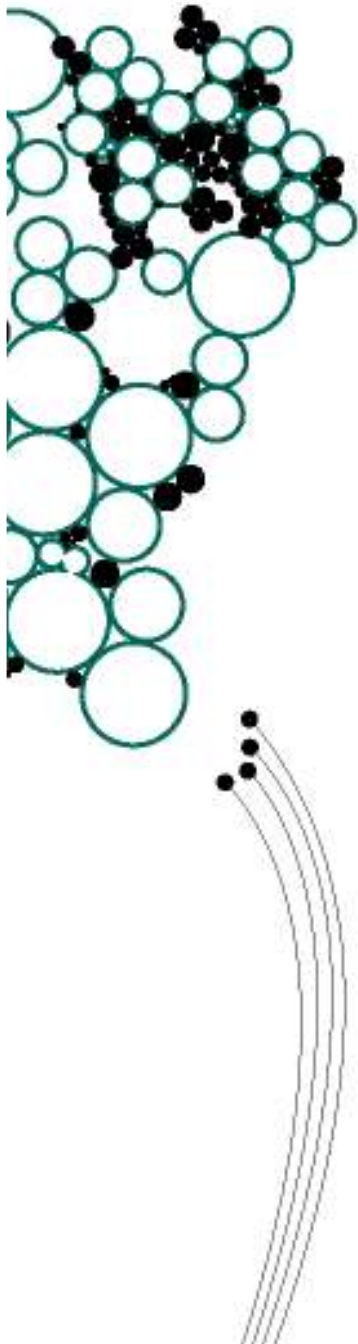
- For 2 and 3 'upgrading' of pyrolysis oil needed
- From 2-3: increase in upgrading severity needed
- Option 2 "Deoxygenation important"



## FCC of Hydrotreated Pyrolysis Oil

- Hydrotreating in autoclave (290 bar)
- MAT tests with 80/20 mixture of long residue and hydrotreated pyrolysis oil (lab-scale)
- Next stage → pilot testing

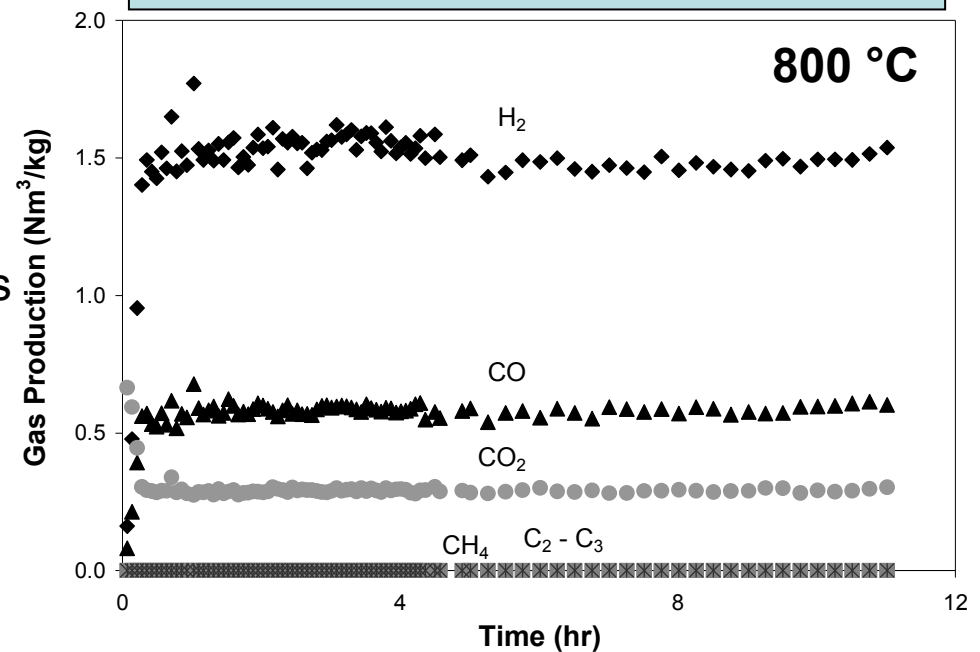
Hydrotreating temp °C		230	260	300	<b>330</b>	340	
Oxygen content oil wt%		28	24.4	22.6	<b>15.5</b>	16.9	
MAT FCC 20 wt% hydrotreated oil 80 wt% long residue							
		<b>Long Residue</b>					
Cat/oil raio		3.1	4.3	3.4	3.4	3.7	3.8
LPG yield		8.5	10.1	9.4	9.6	8.9	9.2
Gasoline yield		<b>44</b>	<b>40.2</b>	<b>41.7</b>	<b>43.4</b>	<b>43.5</b>	<b>43</b>
LCO yield		25.2	21.3	22.2	22.5	23.8	24
Dry gas		1.5	2.3	21.1	1.8	1.9	2
Coke yield		<b>5.9</b>	<b>7.2</b>	<b>6.6</b>	<b>5.2</b>	<b>5.5</b>	<b>5.8</b>
Other (HCO, Slurry Oil)		14.8	10.8	11	11.6	12.2	12
Water		0	7.9	6.7	5.7	3.9	3.9



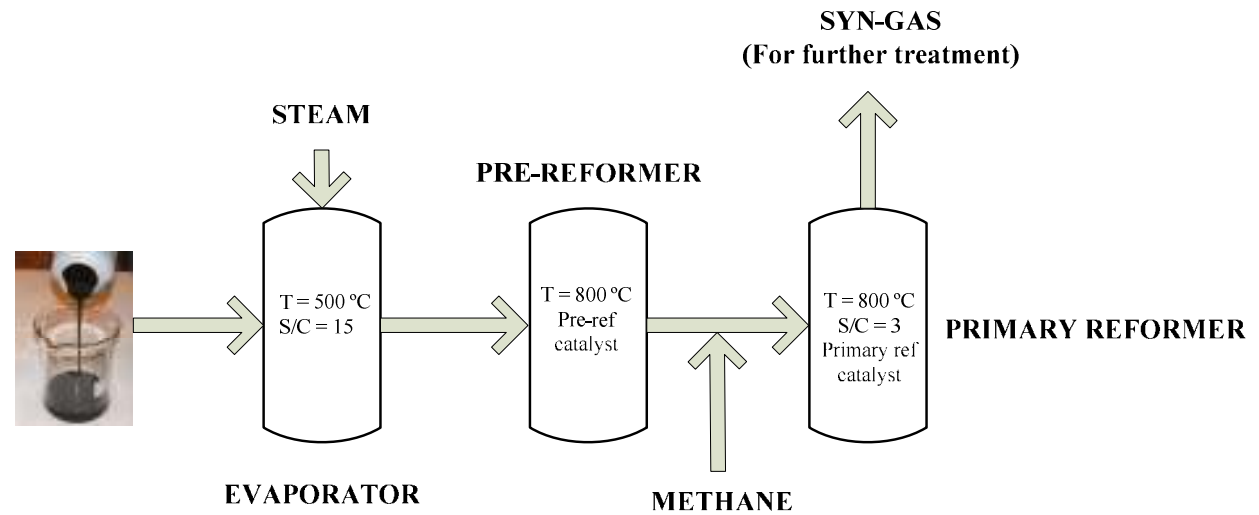
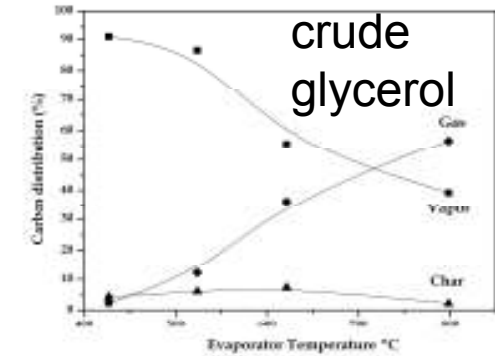
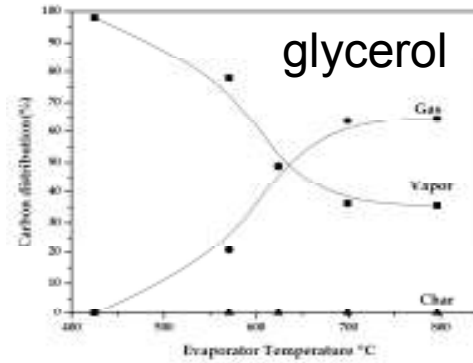
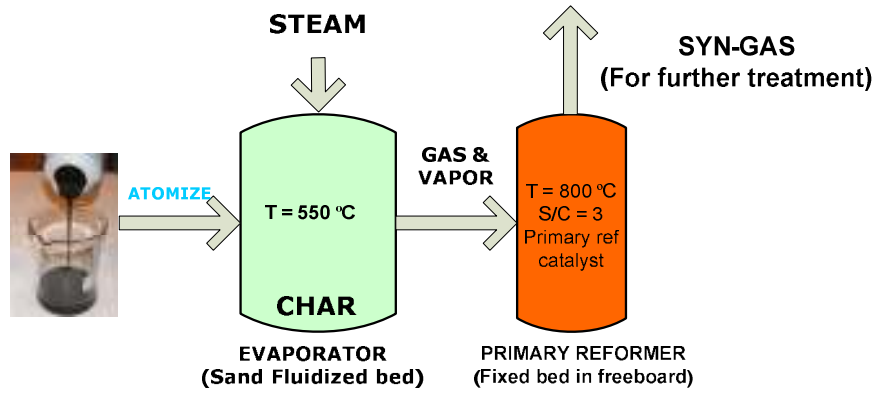
## Gasification Route: Reforming

- Reforming of Biomass
- Biomass + H<sub>2</sub>O → CO + H<sub>2</sub> (Ni)  
(CH<sub>4</sub> + H<sub>2</sub>O → CO + 3H<sub>2</sub>)
- Allows smaller scale operation
  - Lower T
  - No oxygen needed
- R&D phase
  - Severe problems for solid biomass
  - Liquid biomass shows promising results

Catalytic reforming of pyrolysis oil over commercial Ni catalysts

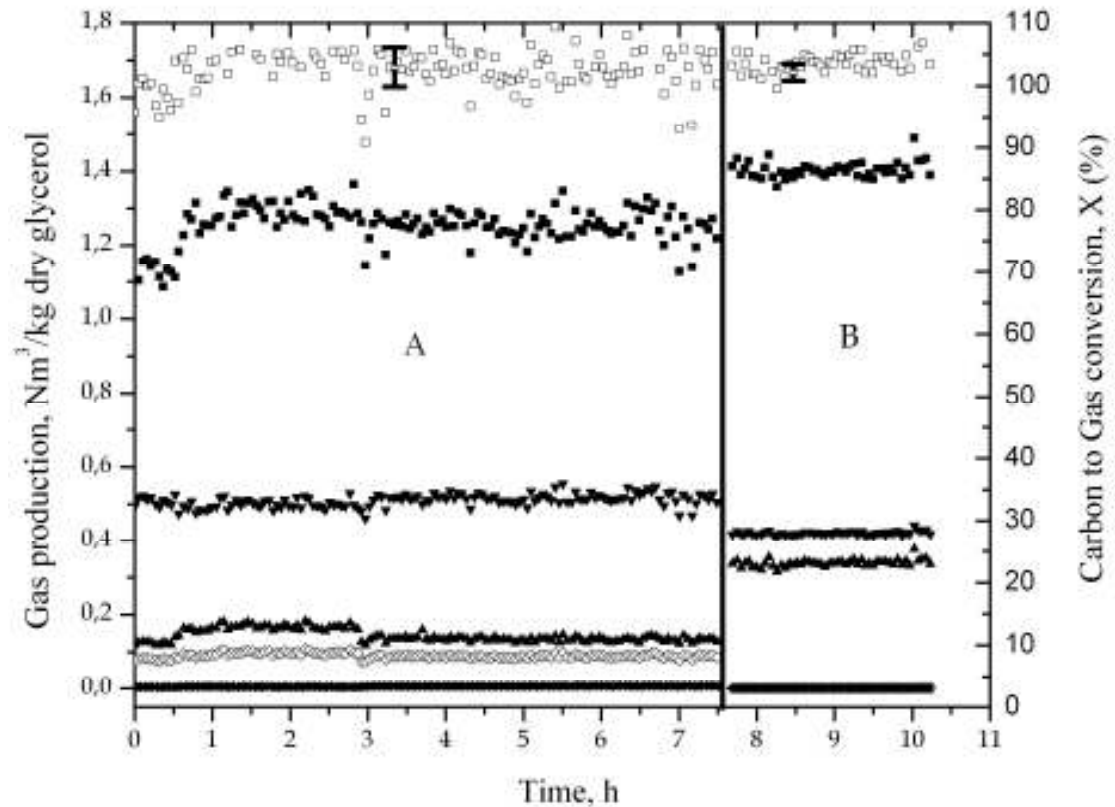


# Hybrid Reforming



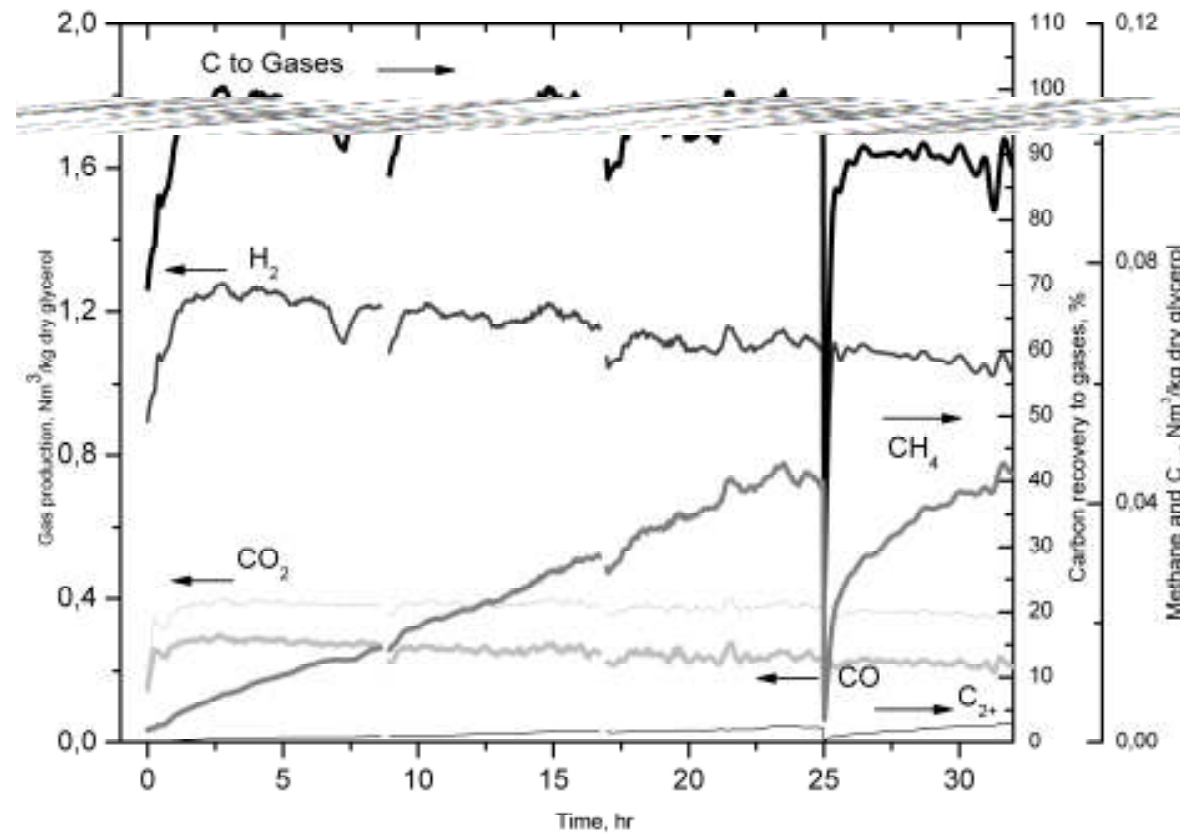


## Glycerol as Feed

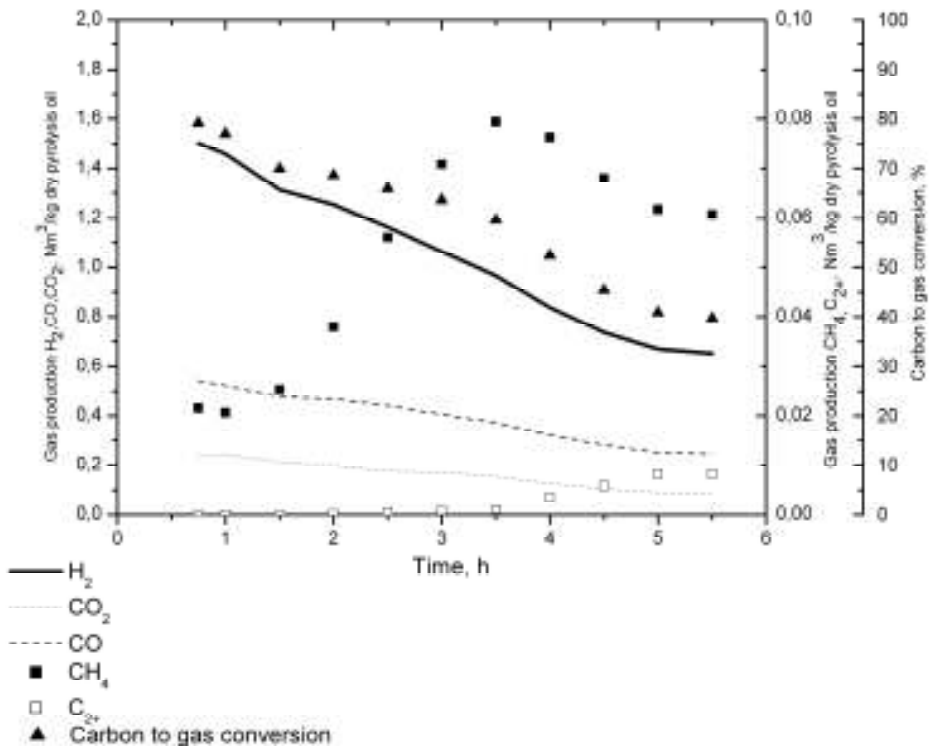
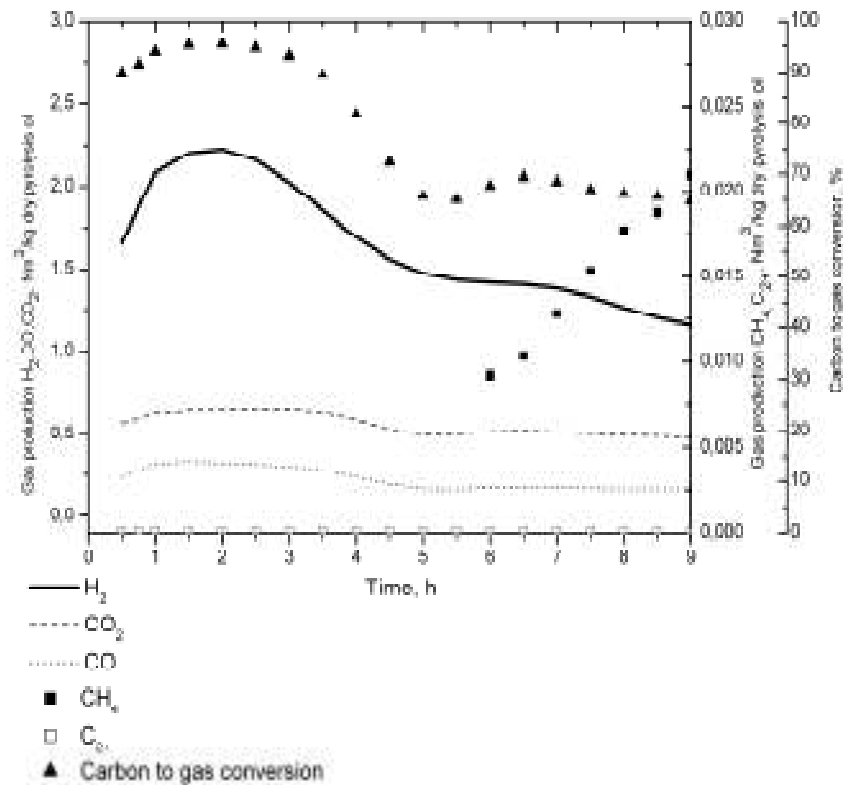


Pre-reforming and steam reforming of glycerol (62.5 wt%). (A)  $S/C = 3$ ,  $T_{cat} = 588^{\circ}\text{C}$  and (B)  $S/C = 3$ ,  $T_{cat} = 787^{\circ}\text{C}$ . For all cases  $GC1HSV = 838 \text{ h}^{-1}$   
□ Carbon to Gas conversion, ■ H<sub>2</sub>, ▼ CO<sub>2</sub>, ▲ CO, ◇ CH<sub>4</sub>

# Crude Glycerol as Feed



# Pyrolysis oil as Feed



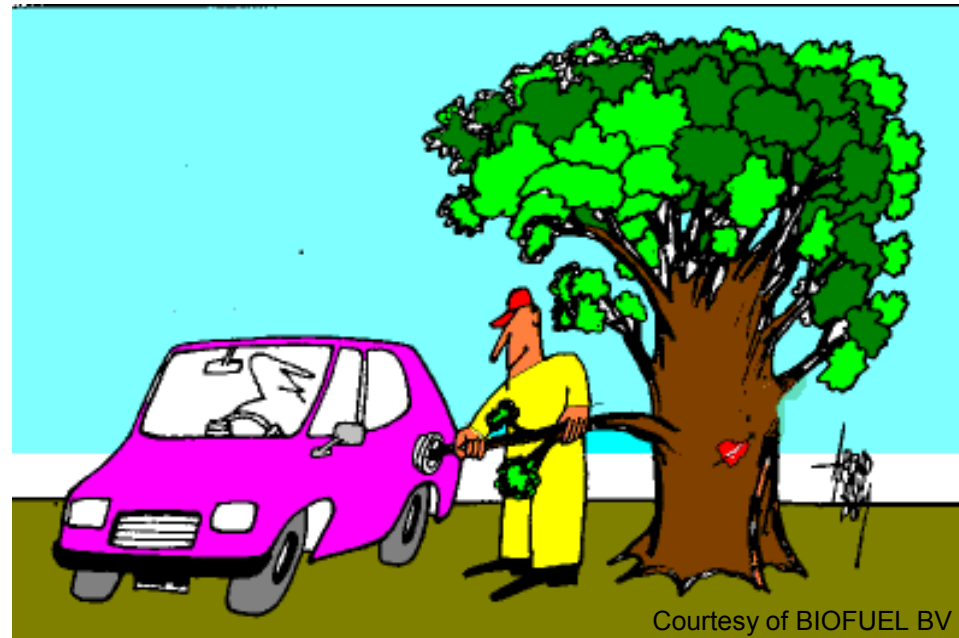


## Concluding Remarks

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- Large volumes of residues can be made available (and scales match with lower limit of fossil feed processing → co-processing)
- Liquid biofuels from forestry, agriculture and paper/pulp residues is the R&D – Demonstration stage (5-10 years for full scale commercial operation)
  - Liquefaction – Refining
  - Gasification – Gas conversion
- Winners (technology level and fuel type) cannot be identified yet, hence, multiple diverse approaches should be investigated.
- For quick introduction of large amounts of biofuels, it is essential to integrate and to partner-up with existing industries and markets.
- For a fast development trajectory it is essential to adapt the knowledge available for making fossil fuels to lignocellulose-based fuels.
  - Catalysis
  - Process Technology

Thanks for your attention!



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